

احداث ردیف تراکم گاز در ایستگاه جمع آوری بینک



شماره پیمان:

.04-.04-.116

CALCULATION NOTE FOR DRUM SIZING							
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه
BK	GCS	PEDCO	120	PR	CN	0002	D05

شماره صفحه: ۱ از ۲۷

طرح نگهداشت و افزایش تولید ۲۷ مخزن

CALCULATION NOTE FOR DRUM SIZING

نگهداشت و افزایش تولید میدان نفتی بینک

Class:2		CLIENT Doc. Number:	F0Z-708740			
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D00	SEP. 2021	IFC	M.Aryafar	M.Fakharian	Sh.Ghalikar	
D01	NOV.2021	IFA	M.Aryafar	M.Fakharian	M.Mehrshad	_
D02	DEC.2021	IFA	M.Aryafar	M.Fakharian	M.Mehrshad	
D03	MAR.2022	IFA	M.Aryafar	M.Fakharian	M.Mehrshad	
D04	JUL.2022	IFA	M.Aryafar	M.Fakharian	M.Mehrshad	
D05	OCT.2022	IFA	M.Aryafar	M.Fakharian	M.Mehrshad	

Status:

IDC: Inter-Discipline Check
IFC: Issued For Comment
IFA: Issued For Approval
AFD: Approved For Design
AFC: Approved For Construction
AFP: Approved For Purchase
AFQ: Approved For Quotation
IFI: Issued For Information
AB-R: As-Built for Client Review
AB-A: As-Built -Approved



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· ۵۳ - · ۷۳ - 9118

CALCULATION NOTE FOR DRUM SIZING							
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه
BK	GCS	PEDCO	120	PR	CN	0002	D05

شماره صفحه: ۲ از ۲۷

REVISION RECORD SHEET

PAGE	D00	D01	D02	D03	D04	D05
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احداث ردیف تراکم گاز در ایستگاه جمع آوری بینک



شماره پیمان:

· 24 - · 74 - 9114

CALCULATION NOTE FOR DRUM SIZING							
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه
BK	GCS	PEDCO	120	PR	CN	0002	D05

شماره صفحه: ۳ از ۲۷

CONTENTS

1.0	NTRODUCTION	4
2.0	SCOPE	4
3.0	NORMATIVE REFERENCES	5
3.1 3.2 3.3 3.4	LOCAL CODES AND STANDARD THE PROJECT DOCUMENTS. ENVIRONMENTAL DATA ORDER OF PRECEDENCE	5 5
4.0	ABBREVIATIONS	
5.0	CALCULATION RESULTS	6
6.0	CLOSE DRAIN DRUM CALCULATION REPORT	6
7.0	DIESEL OIL STORAGE TANK CALCULATION REPORT	7
8.0	AIR RECEIVER VOLUME CALCULATION REPORT	7
9.0	NITROGEN RECEIVER VOLUME CALCULATION REPORT	8
10.0	GLYCOL SUMP DRUM CALCULATION	8
11.0	POTABLE WATER TANK	8
12.0	OILY WATER SUMP	
13.0	GLYCOL STORAG TANK	10
14.0	FLARE DRUM CALCULATION	11
15.0	CALCULATION REPORT	13
ATTAC	CHMENT	13



احداث ردیف تراکم گاز در ایستگاه جمع آوری بینک



شماره پیمان:

.04 - .14 - 414

CALCULATION NOTE FOR DRUM SIZING							
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه
BK	GCS	PEDCO	120	PR	CN	0002	D05

شماره صفحه: ٤ از ٦٧

1.0 NTRODUCTION

Binak oilfield in Bushehr province is a part of the southern oilfields of Iran, is located 20 km northwest of Genaveh city.

With the aim of increasing production of oil from Binak oilfield, an EPC/EPD Project has been defined by NIOC/NISOC and awarded to Petro Iran Development Company (PEDCO). Also PEDCO (as General Contractor) has assigned the EPC-packages of the Project to "Hirgan Energy - Design and Inspection" JV.

As a part of the Project, a New Gas Compressor Station (adjacent to existing Binak GCS) shall be constructed to gather of 15 MMSCFD (approx.) associated gases and compress & transfer them to Siahmakan GIS.

GENERAL DEFINITION

The following terms shall be used in this document.

CLIENT: National Iranian South Oilfields Company (NISOC)

PROJECT: Binak Oilfield Development - Surface Fcilities; New

Gas Compressor Station

EPD/EPC CONTRACTOR (GC): Petro Iran Development Company (PEDCO)

EPC CONTRACTOR: Joint Venture of : Hirgan Energy – Design & Inspection

(D&I) Companies

VENDOR: The firm or person who will fabricate the equipment or

material.

EXECUTOR: Executor is the party which carries out all or part of

construction and/or commissioning for the project.

THIRD PARTY INSPECTOR (TPI): The firm appointed by EPD/EPC CONTRACTOR (GC)

and approved by CLIENT (in writing) for the inspection

of goods.

SHALL: Is used where a provision is mandatory.

SHOULD: Is used where a provision is advisory only.

WILL: Is normally used in connection with the action by

CLIENT rather than by an EPC/EPD CONTRACTOR,

supplier or VENDOR.

MAY: Is used where a provision is completely discretionary.

2.0 SCOPE

This document provides the vessel and drum sizing calculation for BINAK Gas Compressor Station.



احداث ردیف تراکم گاز در ایستگاه جمع آوری بینک



پیمان:	شماره	
پیمان:	شماره	

۹۱۸۴ – ۲۷۰ – ۳۵۰

CALCULATION NOTE FOR DRUM SIZING							
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه
BK	GCS	PEDCO	120	PR	CN	0002	D05

شماره صفحه: ٥ از ٦٧

3.0 NORMATIVE REFERENCES

3.1 Local Codes and Standard

• IPS-E-PR-360 Engineering Standard For Process Requirement Of

Vessels Reactors And Separators

• IPS-E-PR-850 Engineering Standard For Process Design Of Liquid &

Gas Transfer And Storage

3.2 The Project Documents

BK-GCS-PEDCO-120-PR-PF-0001 Process Flow Diagram (PFD)

BK-GNRAL-PEDCO-000-PR-DB-0001 Process Basis of Design

BK-GNRAL-PEDCO-000-PR-DC-0001 Process Design Criteria

3.3 ENVIRONMENTAL DATA

Refer to "Process Basis of Design"; Doc. No. Process Basis of Design BK-00-HD-000-PR-DB-0001

3.4 ORDER OF PRECEDENCE

In case of any conflict between the contents of this document or any discrepancy between this document and other project documents or reference standards, this issue must be reported to the CLIENT. The final decision in this situation will be made by CLIENT.

4.0 ABBREVIATIONS

NIOC: National Iranian Oil Company

NISOC: National Iranian South Oil Company

PFD: Process Flow Diagram

P&ID: Piping and Instrumentation Diagram

BFPD: Barrel Fluid per Day



احداث ردیف تراکم گاز در ایستگاه جمع آوری بینک



	شماره پیمان:
٠٥٣ - ٠٧٣ -	- 9114

	CALCULATION NOTE FOR DRUM SIZING							
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه	
BK	GCS	PEDCO	120	PR	CN	0002	D05	

شماره صفحه: ٦ از ٦٧

5.0 CALCULATION RESULTS

For sizing of equipment's all possible cases have been considered and worst case has been chosen. The details of calculations are presented as follow. List of equipment is summarized in below table: $\begin{array}{c} \\ \\ D05 \end{array}$

Tag Number	Equipment Description	P&ID. N	SIZE (ID*TL-TL)(m)
V-2101	1ST STAGE GAS COMPRESSION SUCTION DRUM	BK-GCS-PEDCO-120-PR-PI-0006	0.9 × 3
V-2102	2ND STAGE GAS COMPRESSION SUCTION DRUM	BK-GCS-PEDCO-120-PR-PI-0009	0.9 × 3
V-2103	GAS COMPRESSION DISCHARGE DRUM	BK-GCS-PEDCO-120-PR-PI-0012	0.9 × 2.84
V-2104	SLUG CATCHER	BK-GCS-PEDCO-120-PR-PI-0004 (1/3)	4.2 × 12.6
V-2105	INLET KNOCK OUT DRUM	BK-GCS-PEDCO-120-PR-PI-0005	1.5 × 4.5
V-2205	FUEL GAS K.O. DRUM	BK-GCS-PEDCO-120-PR-PI-0022	0.438 × 2.95
V-2106	DEGASSING VESSEL	Deleted	Deleted
V-2202	CLOSED DRAIN DRUM	BK-GCS-PEDCO-120-PR-PI-0017(2/2)	2.6 × 7.8
V-2206	DESEL OIL DRUM	BK-GCS-PEDCO-120-PR-PI-0023	2 × 4.75
V-2203	INSTRUMENT AIR RECEIVER	BK-GCS-PEDCO-120-PR-PI-0015(2/2)	1.5×5
V-2204	NITROGEN RECEIVER	BK-GCS-PEDCO-120-PR-PI-0016	1 × 3.15
V-2201	LP FLARE K.O. DRUM	BK-GCS-PEDCO-120-PR-PI-0020(2/3)	1 × 3
V-2107	GLYCOL SUMP DRUM	BK-GCS-PEDCO-120-PR-PI-0025	1.1 × 3.6
T-2101	SLUG STORAGE TANK	Deleted	Deleted
T-2102	LEAN GLYCOL STORAGE TANK	BK-GCS-PEDCO-120-PR-PI-0014	4 × 5
T-2209	POTABLE WATER TANK	BK-GCS-PEDCO-120-PR-PI-0024	3.5 x 2.6
SU-2202	OILY WATER SUMP	BK-GCS-PEDCO-120-PR-PI-0021	3x 3 x 4

6.0 Close drain drum calculation report

For sizing close drain vessel, all continuous and intermittent drain should be investigated and the greatest inventory (V-2104) at a same time should be selected as the basis of drain drum sizing.

Close Drain Drum Calculation						
Drum Diameter	2.6	m				
Drum Length	7.8	m				
Drum Total Volume	46	m ³				
Maximum Continues Inlet Flow	3	m³/hr				
HLL	2.15	m				
LLL	0.3	m				
Liquid Volume HLL	40.9	m ³				
Liquid Volume LLL	2.9	m ³				
Storage Volume (between HLL & LLL)	38	m ³				



احداث ردیف تراکم گاز در ایستگاه جمع آوری بینک



	پیمان:	شماره
٠ ۵٣ - ٠	۷۳ – ۹۱۸۴	

CALCULATION NOTE FOR DRUM SIZING							
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه
BK	GCS	PEDCO	120	PR	CN	0002	D05

شماره صفحه: ۷ از ۹۲

7.0 Diesel oil storage tank calculation report



The Diesel Oil Storage Drum shall be capable to supply fuel oil to all the users for a minimum of 3 days of continuous operation.

Fuel oil storage drum volume is based on corrosion study, fire water pump calculation and diesel generator consumption.

Fuel Oil Storage Drum Calculation						
Drum Diameter	<mark>4.750</mark>	m				
Drum Length	2.0	m				
Drum Total Volume	17.2	m3				
Total Fuel Oil Consumption	5.1	m3/day				
HLL	1.75	m				
LLL	0.15	m				
Vol. from Bottom to HLL	15.85	m3				
Vol. from Bottom to LLL	0.54	m3				
Working Capacity	15.3	m3				

8.0 Air receiver volume calculation report

The air receiver is sized to provide a buffer supply for air of 15 minutes from a pressure of 8 barg down to 4.5 barg, based on the air consumption rate of the plant.

Air receiver						
Barometric Pressure P0	1.03	Bara				
Initial Air Receiver Pressure P1	8	Barg				
Final Air Receiver Pressure P2	4.5	Barg				
Air Receiver Retention time	15	Min				
Total Plant Air Concumption	119.34	Nm³/hr				
Total Plant Air Consumption	125.9	Sm³/hr				
Max. Air Receiver Required Volume	9.3	m ³				
Air Receiver Selected Diameter	1.5	m				
Air Receiver Selected Length	5	m				
Air Receiver Calculated Volume	9.7	m ³				



احداث ردیف تراکم گاز در ایستگاه جمع آوری بینک



	شماره پیمان:
٠٥٣ - ٠٧٣ -	- 9114

CALCULATION NOTE FOR DRUM SIZING							
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه
BK	GCS	PEDCO	120	PR	CN	0002	D05

شماره صفحه: ۸ از ۲۷

9.0 Nitrogen receiver volume calculation report

The nitrogen receiver is sized to provide a buffer supply for 15 minutes from a pressure of 8 barg down to 4 barg, based on the maximum nitrogen consumption rate of the plant.

Nitrogen receiver					
Barometric Pressure PO	1.03	Bara			
Initial N2 Receiver Pressure P1	8	Barg			
Final N2Receiver Pressure P2	4	Barg			
N2 Receiver Retention time	15	Min			
T	43	Nm³/hr			
Total N2 Consumption	45.8	Sm³/hr			
Max. N2 Receiver Required Volume	2.95	m ³			
N2 Receiver Selected Diameter	1	m			
N2 Receiver Selected Length	3.15	m			
N2 Receiver Calculated Volume	3	m ³			

10.0 Glycol sump drum calculation

Glycol Sump Drum Calculation					
Drum Diameter	1.1	m			
Drum Length	3.6	m			
Drum Total Volume	3.77	m ³			
HLL	0.65	m			
LLL	0.3	m			
Liquid Volume HLL	2.33	m ³			
Liquid Volume LLL	0.82	m ³			
Storage Volume (between HLL & LLL)	1.51	m ³			

11.0 POTABLE WATER TANK

Potable Water Tank Calculation					
Tank Diameter	3.5	m			
Tank Height	2.6	m			
Tank Nominal Capacity	25	m ³			
HLL	2.25	m			
LLL	0.15	m			
Working Capacity	20	m ³			



احداث ردیف تراکم گاز در ایستگاه جمع آوری بینک



شما

· 24 - · 74 - 4114

CALCULATION NOTE FOR DRUM SIZING							
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه
BK	GCS	PEDCO	120	PR	CN	0002	D05

شماره صفحه: ۹ از ۲۷

12.0 OILY WATER SUMP



Oily Water Sump					
Hold-Up time	15	m			
Length (L)	3	m			
Hight (H)	3	m			
Width (W)	4	m			
HLL	2.2	m			
Full Volume	30	m			
Usable Volume	26.4	m			



احداث ردیف تراکم گاز در ایستگاه جمع آوری بینک



	شماره پیمان:	
.0404 -	- 9114	

CALCULATION NOTE FOR DRUM SIZING							
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه
BK	GCS	PEDCO	120	PR	CN	0002	D05

شماره صفحه: ۱۰ از ۲۷

13.0 GLYCOL STORAG TANK

TAG NUMBER	TK-2102	DESCRIPTION
Working Capacity (m3)	44	
Discharge Flow rate (m3/h)	5.5	
Estimated Nominal capacity (m3)	62	Should be great that working capacity
Tank Height (selected from table) (m)	5	Refer to TABLE A1 (IPS-E-PR360)
Tank Diameter (selected from table) (m)	4	Refer to TABLE A1 (IPS-E-PR360)
Outlet Nozzle Diameter (in)	2	(Set By Pump Calculation)
Minimum Distance From Bottom Of Tank To Center Of Nozzles(mm)	175	Refer to TABLE 5.6a (API 650)
Selected Distance	250	
Center Of Nozzle(mm)	30	
Value For low low liquid level from top of nozzle	150	minimum 150 mm Refer to (IPS- E-PR-360) section 6.3.1.2.1
calculated low low liquid of tank level (mm)	430	
selected low low liquid of tank level (mm)	600	
Time between low low liquid level and low liquid level (min)	2	usually 2-5 min
volume of liquid between low liquid level and low low liquid level (m3)	0.2	
Height of low liquid level and low low liquid level(mm)	15	
Selected Height of low liquid level and low low liquid level(mm)	200	
Height of high liquid level and low liquid level(mm)	3503	
Time between high high liquid level and high liquid level (min)	2	usually 2-5 min
volume of liquid between high high liquid level and high liquid level (m3)	0.2	
Height of high high liquid level and high liquid level(mm)	15	
Selected Height of high high liquid level and high liquid level(mm)	200	
Heigh between of roof tank and high high liquid level (mm)	450	
Calculated height of tank (m)	5.0	TRUE
RESULTS		1
Tank Height (m)	5	
Tank Diameter (m)	4	
LLL (mm)	600	
LL (m)	800	
HL(m)	4300	
HHL (m)	4500	



احداث ردیف تراکم گاز در ایستگاه جمع آوری بینک



۹۱۸۴ - ۲۷۰ - ۲۵۰

CALCULATION NOTE FOR DRUM SIZING							
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه
BK	GCS	PEDCO	120	PR	CN	0002	D05

شماره صفحه: ۱۱ از ۲۷

14.0 Flare drum calculation

The drum size is based on depressurizing study and result shown as follow:

Project Name: BINAK Gas Compressor Station Item Name : Flare Drum FLARE DRUM CALCULATION _____ **OPERATING DATA** 5.25 Gas mass flow rate,(Kg/s) Gas density T,P (Kg/m3) 2.86 Qg actual volume flow,(m3/s) 1.83 Gas viscosity,(cp) 0.01 Liquid flow rate,(Kg/s) 0.264 Liquid density T,P (Kg/m3) 846.2 0.000 QI actual volume flow,(m3/s) 600.0 Particle size, (microns) Number of vapor pass 1 10 Over design factor,(%) **CALCULATION RESULTS** Ud, Dropout Velocity(m/s) 1.9830 $CR_e^2 = \frac{0.13 \times 10^8 \times D^3 \times (\rho_I - \rho_v)}{\mu^2}$ C(Re)2 86870.9 From API-521 Fig.9 C, Drag coefficient 0.58 DRUM SIZING CRITERIA R.min mm hv HHLL h1 2 100 HLL h2 30 300 2 LLL h3 100 LLLL 150 h4 Bt. 0



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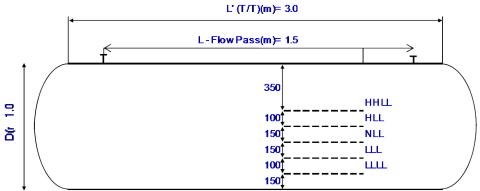
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CALCULATION NOTE FOR DRUM SIZING								
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه	l
BK	GCS	PEDCO	120	PR	CN	0002	D05	l
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شماره صفحه: ۱۲ از ۲۷

CALCULATION	RESULTS				
		Trial.1	Trial.2	Trial.3	Trial.4
Assumed dia	meter (m)	6	1	1.1	1.2
Assumed Leng	th (m)	2.5	2.4	2.5	2.2
Added Length		0.6	0.6	0.6	0.6
At, Total area(r	m2)	28.27	0.79	0.95	1.13
Av, Vapor area	(m2)	26.62	0.24	0.37	0.51
Ah1, Liquid are	a(m2)	0.36	0.10	0.11	0.12
Ah2, Liquid are	a(m2)	0.89	0.29	0.31	0.33
Ah3, Liquid are	a(m2)	0.21	0.08	0.08	0.09
Ah4, Liquid are	a(m2)	0.19	0.07	0.08	0.08
ht (Cm)		600	100	110	120
hv(ht-HI1) (Cm)		535	35	45	55
hL1(HH)(Cm)		65	65	65	65
hL2(H)(Cm)		55	55	55	55
hL3(L)(Cm)		25	25	25 15	25 15
h4(LL)(Cm)		15	15		
Liquid drop out	time,(sec)	2.70	0.18	0.23	0.28
Vapor velosity	(m/s)	0.08	8.24	5.52	3.99
L, Flowpath length(m)		0.2	1.5	1.3	1.1
3 <l d<4<="" td=""><td>0.5</td><td>3.0</td><td>2.8</td><td>2.4</td></l>		0.5	3.0	2.8	2.4
Stimated Weight (kg)		1568	249	283	279
% Total area (v	rapor)	94	31	38	45
Selected Ler	igth (m)	3.1	3.0	3.1	2.8
		Trial. 1	Trial.2	Trial.3	 Trial.4
Top. (mm)	hv	5350	350	450	550
HHLL (mm)	h1	100	100	100	100
HLL (mm)	h2	300	300	300	300
LLL (mm)	h3	100	100	100	100
LLLL (mm)	h4	150	150	150	150
Bt.	-				





احداث ردیف تراکم گاز در ایستگاه جمع آوری بینک



شماره پیمان:

· ۵۳ - · ۷۳ - 9 1 1 4

CALCULATION NOTE FOR DRUM SIZING								
پروژه	بسته کاری	صادر کننده	تسهيلات	رشته	نوع مدرك	سريال	نسخه	l
BK	GCS	PEDCO	120	PR	CN	0002	D05	

شماره صفحه: ۱۳ از ۲۷

15.0 Calculation Report



ATTACHMENT

(SOFTWARE RESULT)