

C-2101-D1 A/B/C
1ST STAGE SUCTION
SNUBBER
OP. TEMP.: 18.9 ~ 36.8 °C
OP. PRESS.: 4.9 BARG

C-2101-D2 A/B/C
1ST STAGE DISCHARGE
SNUBBER
OP. TEMP.: 116 ~ 129 °C
OP. PRESS.: 17.9 BARG

C-2102-D1 A/B/C
2ND STAGE SUCTION
SNUBBER
OP. TEMP.: 59.9 °C
OP. PRESS.: 17 BARG

C-2102-D2 A/B/C
2ND STAGE DISCHARGE
SNUBBER
OP. TEMP.: 148 ~ 149 °C
OP. PRESS.: 54.8 BARG

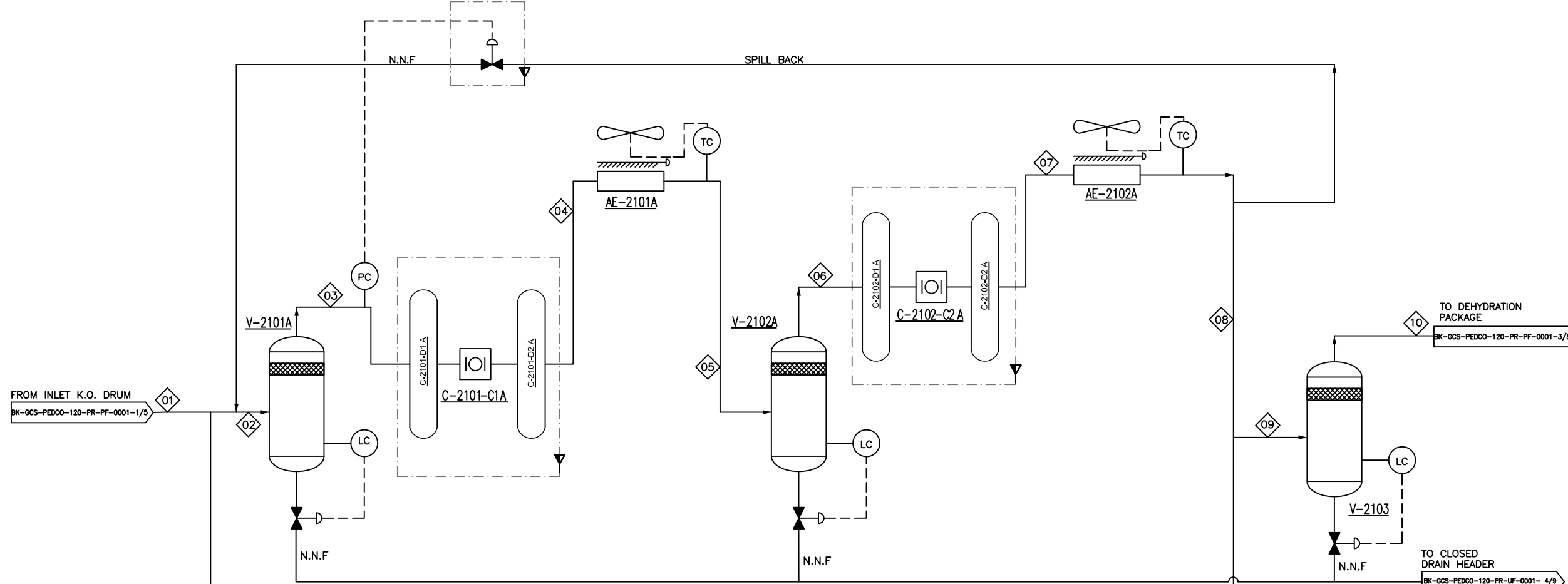
V-2101 A/B/C
1ST STAGE GAS
COMPRESSION SUCTION DRUM
OP. TEMP.: 19 ~ 36.9 °C
OP. PRESS.: 5.1 BARG

AE-2101 A/B/C
1ST STAGE GAS
COMPRESSION AIR COOLER
INLET. TEMP.: 116 ~ 129 °C
OUTLET. TEMP.: 60 °C

V-2102 A/B/C
2ND STAGE GAS
COMPRESSION SUCTION DRUM
OP. TEMP.: 60 °C
OP. PRESS.: 17.2 BARG

AE-2102 A/B/C
2ND STAGE GAS
COMPRESSION AIR COOLER
INLET. TEMP.: 148 ~ 149 °C
OUTLET. TEMP.: 60 °C

V-2103
2ND STAGE GAS
DISCHARGE DRUM
OP. TEMP.: 60 °C
OP. PRESS.: 54.1 BARG



NOTE 2

NOTE 2,3

LP SECTION TRAIN B
(IDENTICAL TO TRAIN A)

HP SECTION TRAIN B
(IDENTICAL TO TRAIN A)

LP SECTION TRAIN C
(IDENTICAL TO TRAIN A)

HP SECTION TRAIN C
(IDENTICAL TO TRAIN A)

C-2101-C1 A/B/C
1ST STAGE GAS
COMPRESSOR
RATED CAPACITY: 8162.9 / 8343.5 NM3/HR
DIFF. PRESS.: 13 BAR
BKW: 441.1 / 435.2 KW

C-2102-C2 A/B/C
2ND STAGE GAS
COMPRESSOR
RATED CAPACITY: 8162.9 / 8343.5 NM3/HR
DIFF. PRESS.: 37.8 BAR
BKW: 450.8 / 468.5 KW

REFERENCE DRAWINGS												A3
Symbol & Legend For PFD and P&ID												DWG. NUMBER
BK-GHRAI-PEDCO-000-PR-P1-0001												

- Note :
- 2+1 TRAIN IS CONSIDERED.
 - TRAIN "B" , "C" ARE THE SAME AS TRAIN "A" .
 - TRAIN "C" IS STAND BY.

Legend :

◇ STREAM NUMBER

V05	OCT. 2024	IFI	HAVAYAR CO.	M.FAKHARIAN	M.SADEGHIAN	
V04	MAY 2024	IFI	HAVAYAR CO.	M.FAKHARIAN	S.FARAMARZPOUR	
V03	FEB. 2024	IFI	HAVAYAR CO.	M.FAKHARIAN	S.FARAMARZPOUR	
V02	NOV. 2023	IFI	HAVAYAR CO.	M.FAKHARIAN	S.FARAMARZPOUR	
V01	SEP. 2023	IFI	HAVAYAR CO.	M.FAKHARIAN	S.FARAMARZPOUR	
V00	MAY. 2023	IFI	HAVAYAR CO.	M.FAKHARIAN	A.M. MOHSENI	
REV.	DATE	P.O.I.	PREP.	CHK.	APP.	AUT.

PROJECT NAME:		BINAK OILFIELD DEVELOPMENT SURFACE WORK PACKAGES	
PROJECT NO.:		---	
EPC CONTRACTOR:		EPC/EPD CONTRACTOR:	
 HIRGAN ENERGY - DESIGN & INSPECTION COMPANIES		 PETROIRAN DEVELOPMENT COMPANY	

REV.	DESCRIPTION	BY	DATE	BY	DATE
		CHECKED		REV.	APPR.
اسلامی و دولتی مجوزوں کی بنیاد پر یہ نقشہ تیار کیا گیا ہے۔ اس کے حقوق محفوظی کے لئے اس کا استعمال اور اس کے کاپیوں کو دوسروں کو پیش کرنا ممنوع ہے۔					
					
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BINAK OILFIELD DEVELOPMENT SURFACE WORK PACKAGES					
DATE	SCALE	DRAWING BY	CHECKED BY	PROJECT ENG.	
NO CONSTRUCTION PERMITTED UNLESS DRAWING APPROVED					
APPROVED FOR CONSTRUCTION		BY:		DATE:	
BUDGET REF.	LOCATION	SIZE	CLASS	SERIAL NO.	SHEET
					REVISION



SUMMER CASE											
STREAM NO.	UNIT	01	02	03	04	05	06	07	08	09	10
VAPOR FRACTION		1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00
TEMPERATURE	°C	36.9	36.9	36.8	129	60	59.9	148	60	60	59.9
PRESSURE	BARG	5.1	5.1	4.9	17.9	17.2	17	54.8	54.1	54.1	53.9
MASS FLOW	KG/H	17833	8664	8664	8664	8664	8664	8664	8664	17327	17252
COMPOSITION (MOLE FRACTION)											
H2O		0.0103	0.0103	0.0103	0.0103	0.0103	0.0103	0.0103	0.0103	0.0103	0.0045
CO2		0.0316	0.0316	0.0316	0.0316	0.0316	0.0316	0.0316	0.0316	0.0316	0.0318
H2S		0.0541	0.0541	0.0541	0.0541	0.0541	0.0541	0.0541	0.0541	0.0541	0.0544
METHANE		0.6389	0.6389	0.6389	0.6389	0.6389	0.6389	0.6389	0.6389	0.6389	0.6427
ETHANE		0.1375	0.1375	0.1375	0.1375	0.1375	0.1375	0.1375	0.1375	0.1375	0.1383
PROPANE		0.0773	0.0773	0.0773	0.0773	0.0773	0.0773	0.0773	0.0773	0.0773	0.0778
i–BUTANE		0.0084	0.0084	0.0084	0.0084	0.0084	0.0084	0.0084	0.0084	0.0084	0.0084
n–BUTANE		0.0186	0.0186	0.0186	0.0186	0.0186	0.0186	0.0186	0.0186	0.0186	0.0187
i–PENTANE		0.007	0.007	0.007	0.007	0.007	0.007	0.007	0.007	0.007	0.007
n–PENTANE		0.0038	0.0038	0.0038	0.0038	0.0038	0.0038	0.0038	0.0038	0.0038	0.0038
n–HEXANE		0.0065	0.0065	0.0065	0.0065	0.0065	0.0065	0.0065	0.0065	0.0065	0.0066
n–HEPTANE		0.002	0.002	0.002	0.002	0.002	0.002	0.002	0.002	0.002	0.002
n–OCTANE		0.0006	0.0006	0.0006	0.0006	0.0006	0.0006	0.0006	0.0006	0.0006	0.0006
n–NONANE		0.0003	0.0003	0.0003	0.0003	0.0003	0.0003	0.0003	0.0003	0.0003	0.0003
n–DECANE		0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
NITROGEN		0.003	0.003	0.003	0.003	0.003	0.003	0.003	0.003	0.003	0.003

WINTER CASE											
STREAM NO.	UNIT	01	02	03	04	05	06	07	08	09	10
VAPOR FRACTION		1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00
TEMPERATURE	°C	19	19	18.9	116	60	59.9	149	60	60	59.9
PRESSURE	BARG	5.1	5.1	4.9	17.9	17.2	17	54.8	54.1	54.1	53.9
MASS FLOW	KG/H	15677	7585	7585	7585	7585	7585	7585	7585	15171	15171
COMPOSITION (MOLE FRACTION)											
H2O		0.0036	0.0036	0.0036	0.0036	0.0036	0.0036	0.0036	0.0036	0.0036	0.0036
CO2		0.0252	0.0252	0.0252	0.0252	0.0252	0.0252	0.0252	0.0252	0.0252	0.0252
H2S		0.0471	0.0471	0.0471	0.0471	0.0471	0.0471	0.0471	0.0471	0.0471	0.0471
METHANE		0.7398	0.7398	0.7398	0.7398	0.7398	0.7398	0.7398	0.7398	0.7398	0.7398
ETHANE		0.1143	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143	0.1143
PROPANE		0.0474	0.0474	0.0474	0.0474	0.0474	0.0474	0.0474	0.0474	0.0474	0.0474
i–BUTANE		0.0039	0.0039	0.0039	0.0039	0.0039	0.0039	0.0039	0.0039	0.0039	0.0039
n–BUTANE		0.0081	0.0081	0.0081	0.0081	0.0081	0.0081	0.0081	0.0081	0.0081	0.0081
i–PENTANE		0.0031	0.0031	0.0031	0.0031	0.0031	0.0031	0.0031	0.0031	0.0031	0.0031
n–PENTANE		0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015	0.0015
n–HEXANE		0.0022	0.0022	0.0022	0.0022	0.0022	0.0022	0.0022	0.0022	0.0022	0.0022
n–HEPTANE		0.0006	0.0006	0.0006	0.0006	0.0006	0.0006	0.0006	0.0006	0.0006	0.0006
n–OCTANE		0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
n–NONANE		0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001	0.0001
n–DECANE		0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
NITROGEN		0.003	0.003	0.003	0.003	0.003	0.003	0.003	0.003	0.003	0.003

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V00	MAY. 2023	IFI	HAVAYAR CO.	M.FAKHARIAN	A.M. MOHSENI	
REV.	DATE	P.O.I.	PREP.	CHK.	APP.	AUT.
PROJECT NAME: BINAK OILFIELD DEVELOPMENT SURFACE WORK PACKAGES						
PROJECT NO.: ---						
EPC CONTRACTOR:			EPC/EPD CONTRACTOR:			
 HIRGAN ENERGY – DESIGN & INSPECTION COMPANIES			 PETROIRAN DEVELOPMENT COMPANY			
DRAWING TITLE: PROCESS FLOW DIAGRAM						
SCALE	SIZE	DRAWING NO.			SHEET NO.	REV.
N.T.S.C.	A3	BK–GCS–HY–120–PR–PF–0001			2 OF 2	V05
1	6	1	7	18	19	

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**BINAK OILFIELD DEVELOPMENT
SURFACE WORK PACKAGES**

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BUDGET REF.	LOCATION	SIZE	CLASS	SERIAL NO.	SHEET	REVISION

Note :
1– THE OUTLET TEMPERATURE OF PROCESS GAS FROM INTER STAGE AND AFTER AIR COOLERS SHALL BE 60 °C

Legend :